#### 16.512, Rocket Propulsion Prof. Manuel Martinez-Sanchez Lecture 6: Heat Conduction: Thermal Stresses

#### Effect of Solid or Liquid Particles in Nozzle Flow

An issue in highly aluminized solid rocket motors.

$$2\mathsf{AI} + \frac{3}{2}\mathsf{O}_2 \to \mathsf{AI}_2\mathsf{O}_3$$

m.p. 2072°C, b.p. 2980°C

In modern formulations, with ~ 20% Al by mass, the  $AI_2O_3$  mass fraction of the exhaust can be 35-40%. This material <u>does not expand</u>, so there must be a loss in exit velocity, hence in  $I_{sp}$ .

Assume mass flows mg (gas) ms (solids), non-converting.

The momentum equation is

$$\mathbf{\dot{m}_{g}} \, du_{g} + \mathbf{\dot{m}_{s}} \, du_{s} + Adp = 0$$

Call  $\rho_s$  the (mass of solids)/(volume) (not the density of the solid, theory)

$$\rho_{\rm g}\,u_{\rm g}\,du_{\rm g}+\rho_{\rm s}\,u_{\rm s}\,du_{\rm s}+dp=0$$

Define a mass flux function

$$x = \frac{\dot{m}_{s}}{\dot{m}_{g} + \dot{m}_{s}} = \frac{\rho_{s}u_{s}}{\rho_{g}u_{g} + \rho_{s}u_{s}}$$
$$\Rightarrow \rho_{g}u_{g}\left(du_{g} + \frac{x}{1 - x}du_{s}\right) + dp = 0$$
$$u_{g}du_{g} = -\frac{dp}{\rho_{g}} - \frac{x}{1 - x}u_{g}du_{s}$$

The energy equation is similarly,

$$(1-x)(c_{pg}dT_{g}+u_{g}du_{g})+x(c_{s}dT_{s}+u_{s}du_{s})=0$$

Substitute here ugdug from above:

$$c_{pg}dT_{g} - \frac{dp}{\rho_{g}} - \frac{x}{1-x}u_{g}du_{s} + \frac{x}{1-x}(c_{s}dT_{s} + u_{s}du_{s}) = 0$$

$$\frac{dp}{\rho_{g}} = c_{pg}dT_{g} + \frac{x}{1-x} \Big[ c_{s}dT_{s} + (u_{s} - u_{g})du_{s} \Big]$$

with no particles (x=0), this gives  $R_gT \frac{dp}{P} = c_p dT \rightarrow \frac{P}{P_0} = \left(\frac{T}{T_0}\right)^{\gamma/\gamma-1}$ 

With particles, we need to know the history of the <u>velocity slip</u>  $u_s - u_g$  and of the <u>temperature slip</u>  $T_s - T_g$ . This is a difficult problem, requiring detailed modeling of the motion and heating/cooling of the particle. But we can look at the extreme cases easily.

(a) <u>Very Small Particles</u> → good contact. For sub-micro particles (not a bad representation of reality), we can say that

$$\begin{split} &u_{s} \simeq u_{g} = u, \\ &T_{s} \simeq T_{g} = T \text{ . Then} \\ &\frac{dp}{\rho_{g}} = \left(c_{pg} + \frac{x}{1-x}c_{s}\right)dT \end{split}$$

Note that the mean specific heat (c\_{pg} and c\_{s} are per unit mass) is

and also 
$$\vec{c}_{p} = (1-x)c_{pg} + xc_{s}$$
  
 $\vec{c}_{v} = (1-x)c_{vg} + xc_{s}$   $\vec{R}_{g} = \vec{c}_{p} - \vec{c}_{v} = (1-x)(c_{pg} - c_{vg}) = (1-x)R_{g}$ 

So that 
$$\frac{dp}{\rho_g} = \frac{\bar{c}_p}{1-x} dT$$

$$R_{g}T \frac{dp}{P} = \frac{\overline{c}_{p}}{1-x} dT \rightarrow \frac{dp}{P} = \frac{\overline{c}_{p}}{R_{g}} \frac{dT}{T}$$

and defining an effective  $\bar{\gamma}$  by the usual  $\bar{\gamma} = \frac{\bar{c}_p}{\bar{c}_v}$ ,

$\boxed{\frac{P}{P_0} = \left(\frac{T}{T_0}\right)^{\frac{\bar{\gamma}}{\bar{\gamma}-1}}}$
--

The equation of motion is now

$$\left(\rho_{\rm g}+\rho_{\rm s}\right)$$
udu + dp = 0

Or

$$\frac{\rho_{g}}{1-x}udu + dp = 0$$

$$\frac{\rho_{g}}{1-x} = \frac{P}{R_{g}T(1-x)} = \frac{P}{\overline{R}_{g}T}$$

$$\frac{P}{\overline{R}_{g}T}udu + dp = 0$$

From the two boxed equations we see that <u>everything</u> from here can proceed as if the gas were simple, but with molecular mass

$$\overline{M} = \frac{M_g}{1-x}$$

(or 
$$\overline{R}_g = (1 - x)R_g$$
),

and with

$$\stackrel{-}{c}_{p} = \left(1-x\right)c_{pg} + x\,c_{s}\;. \label{eq:cp_p}$$

For example,

$u_e = \sqrt{2 \frac{1}{\frac{1}{\gamma}}}$	$\frac{1}{1}\overline{R}_{g}T_{c}\left[1-\left(\frac{P_{c}}{P_{c}}\right)\right]$	$\frac{\bar{\gamma}-1}{\bar{\gamma}}$
$u_e = \sqrt{2 - \frac{\gamma}{\gamma}}$	$-1$ $k_g r_c \left[ 1 - \left( \frac{1}{P_c} \right) \right]$	

 $\rm T_{c}$  ,  $\rm P_{c}\,$  in chamber etc.

For sensitivity analysis it may be of interest to linearize this for  $x \ll 1$ . The algebra is tedious, but one gets,

$$\left| \frac{u_e}{u_{e_0}} \cong 1 - \frac{1}{2} \times \left\{ 1 - c \left[ 1 + \frac{\left(1 - \eta_0\right) ln \left(1 - \eta_0\right)}{\eta_0} \right] \right\}$$

with 
$$c = \frac{c_{ps}}{c_{pg}}$$
,  $\eta_0 = 1 - \left(\frac{P_e}{P_c}\right)^{\frac{\gamma-1}{\gamma}}$ 

and, of course,

$$u_{e_0} = \sqrt{2\frac{\gamma}{\gamma-1}}R_gT_c\left[1-\left(\frac{P_e}{P_c}\right)^{\frac{\gamma}{\gamma-1}}\right]$$

We see from this that if c  ${}_{<}1$  (c\_{ps} {}\_{\sim}c\_{pg}, which is common), then u\_e < u\_{e\_0} (and vice-versa).

For a numerical example, look at Problem 2 (attached)

(b) <u>Very Large Particles</u> Hard to quantify, but probably for diameter  $>100\,\mu m$  or

so, the particles have too much inertia (and thermal inertia) to follow the gas acceleration and cooling. We then have

 $du_{s}\ll du_{g}\,; \qquad T_{s}\,\simeq\,T_{c}\,$  (  $\cong\,T_{g}\,$  at chamber)

or  $du_s \simeq 0$ ;  $dT_s \simeq 0$ 

Returning to the  $\frac{dp}{\rho_g}$  equation, it now looks <u>as if there were no particles</u>:

$$\frac{dp}{\rho_{g}} = c_{pg} dT_{g}$$

(i.e. , particles just do not participate in the dynamics or in the thermal balances). So, we still have  $\frac{P}{P_0} = \left(\frac{T}{T_0}\right)^{\gamma/\gamma-1}$ . This does not mean zero performance effect, though. We do not get the full <u>gas</u> exit velocity

$$u_{e} = \sqrt{2 \frac{\gamma}{\gamma - 1} R_{g} T_{c} \left[ 1 - \left( \frac{P_{e}}{P_{c}} \right)^{\gamma - 1/\gamma} \right]}$$

but the particulates do not contribute to thrust, because they exit at  $u_{s} \ll u_{e}\,$  :

$$g I_{sp} = \frac{\dot{m}_g u_e + \dot{m}_s u_s}{\dot{m}_g + \dot{m}_s} = (1 - x)g I_{sp_0}$$

This is actually <u>more</u> loss than in the small particle case (about twice as much, depending on c).

From the example, this is a serious loss in solid rockets.

# Criterion for Slip

$$\frac{4}{3}\pi R_p^3 \rho_s^2$$

$$\int_{m_p} \frac{du_p}{dt} = 6\pi \mu_g R_p \left( u_g - u_p \right) \left\| \frac{2}{9} \frac{R_p^2 \rho_s}{\mu_g} \frac{du_p}{dt} = u_g - u_p \quad \tau_R = \frac{2}{9} \frac{\rho_s R_p^2}{\mu_g}$$

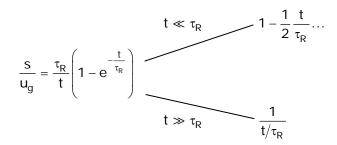
$$\frac{du_p}{dt} = \frac{u_g - u_p}{\tau_R} \quad \text{call } u_g - u_p = s \qquad u_p = u_g - s$$

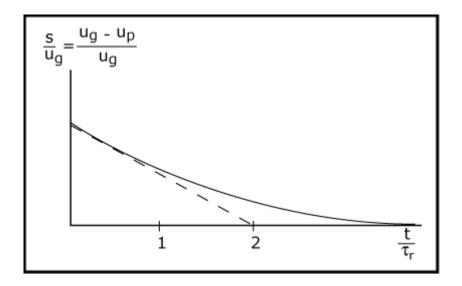
du <sub>g</sub>	ds	S	$\frac{ds}{ds} + \frac{s}{ds}$	_ du <sub>g</sub>
dt			$\frac{dt}{dt} + \frac{\tau_R}{\tau_R}$	

Say 
$$\tau_R$$
 and  $\frac{du_g}{dt} = a_g$  are constant  $\rightarrow s \approx a_g \tau_R + C e^{-\frac{t}{\tau_R}}$   
 $s(0) = 0 \rightarrow C = -a_g \tau_R$ 

$$=\frac{1-\left(1-\epsilon+\frac{\epsilon^2}{2}\dots\right)}{\epsilon}=1-\frac{\epsilon}{2}+\dots$$
  
$$s=a_g\tau_R\left(1-e^{-\frac{t}{\tau_R}}\right)$$

and  $u_g = a_g t$ 





So, small slip for  $t \gg \tau_R$ 

 $\frac{L}{u} \gg \tau_R$ 

$$\frac{L}{u_g} \gg \frac{2}{9} \frac{\rho_s R_p^2}{\mu_g}$$

$$R_p \ll \sqrt{\frac{9}{2} \frac{\mu_g L}{\rho_s \, u_g}}$$

Say  

$$\mu_{g} \sim 3 \times 10^{-5} \text{ Kg/m/s}$$

$$L \sim 0.3 \text{ m}$$

$$\rho_{s} \sim 3 \times 10^{3} \text{ Kg/m}^{3}$$

$$u_{g} \sim 1.5 \times 10^{3} \text{ m/s}$$

$$R_{p} \ll \sqrt{4.5 \frac{\cancel{2} \times 10^{-5} \times 0.3}{\cancel{2} \times 10^{3} \times 1.5 \times 10^{3}}} = \sqrt{0.9 \times 10^{-11}} = 3 \times 10^{-6} \text{ m} = 3 \mu \text{ m}$$

So, 
$$\begin{vmatrix} R_p \ll 3\mu m \rightarrow no \ slip \\ R_p \gg 3\mu m \rightarrow full \ lag$$

# Problems

# Problem 2

As noted in class, the effect of carrying a mass fraction x of fine solid particles in the expanding gas in a rocket nozzle can be accounted for by using an average specific heat ratio

$$\overline{\gamma} = \frac{\left(1 - x\right)c_{pg} + xc_s}{\left(1 - x\right)c_{vg} + xc_s}$$

and an average molecular mass

$$\overline{M} = \frac{M_g}{1-x}$$

For  $AI_2O_3$  the high temperature specific heat is  $c_s = 1260 J/Kg/K$ .

Consider a solid rocket with  $\gamma = 1.17 (1.25)$ ,  $P_e/P_c = 0.01$ ,  $\overline{M}_g = 18 g / \text{mol.}$ For a 20% aluminum loading in the propellant, x is of the order of 37%. Calculate the matched specific impulse of the rocket and compare to what it would be for the same  $T_c = 3300 K$ , but with no particles.

#### Problem 2

Specific heat of clean gas

$$c_{pg} = \frac{r}{r-1} \frac{R}{M} = \frac{\frac{1.25}{0.17}}{\frac{0.17}{0.25}} \frac{8.314}{0.018} = \frac{3180}{2309} \text{ J/Kg/K}$$
$$c_{vg} = \frac{c_{pg}}{r} = \frac{\frac{3180}{1.17}}{\frac{2309}{1.25}} \frac{1.25}{1.25}}{\frac{2718}{1.845}} \text{ J/Kg/K}$$

The specific heat of the solid (or liquid)  $Al_2O_3$  is  $c_s = 1260 \text{ J/Kg/K}$ .

The average specific heat ratio is then

$$\bar{r} = \frac{(1-x)c_{pg} + xc_{s}}{(1-x)c_{vg} + xc_{s}} = \frac{(1-0.37) \times 3180 + 0.37 \times 1260}{(1-0.37) \times 2718 + 0.37 \times 1260} = \frac{1.1336}{1.1795}$$

And the average molecular mass (M\_s  $\simeq \infty$  ) is

$$\overline{M} = \frac{M_g}{1 - x} = \frac{18}{1 - 0.37} = 28.57 \text{ g/mol}$$

The exit speed for  $\frac{P_e}{P_c}$  = 0.01 and  $T_c$  = 3300K is then

$$u_{e} = \sqrt{2\frac{\bar{\gamma}}{\bar{\gamma}-1}\frac{Q}{\overline{M}}T_{c}\left[1-\left(\frac{P_{e}}{P_{c}}\right)^{\frac{\bar{\gamma}-1}{\bar{\gamma}}}\right]} = 2613 \text{ m/sec}$$
2521

NOTE: Alternatively, and easier to do, you can use

$$u_{e} = \sqrt{2 \overline{C}_{p} T_{c} \left[ 1 - \left(\frac{P_{e}}{P_{c}}\right)^{\frac{\overline{\gamma}-1}{\overline{\gamma}}} \right]}$$

with  $\overline{C}_{p} = (1 - 0.37)3180 + 0.37 \times 1260 = 2469 \text{ J/Kg/K}$ 

(so  $\overline{M}$  is not really needed)

As a check,

$$\frac{\gamma}{\overline{\gamma}-1} \frac{R}{\overline{M}} = \frac{1.1336}{0.1336} \frac{8.314}{0.02857} = 2469 \text{ J/Kg/K}$$

as it should.

Under pressure-matched conditions, there is no exit pressure contribution to thrust or  ${\rm I}_{\rm sp}$  , and hence

$$I_{sp} = \frac{2613}{9.81} = 266.3 \text{ sec}$$
257.3 s

Without particulate but with the same  $\rm P_{c}$  ,  $\rm P_{e}~$  and  $\rm T_{c}$  , we would obtain

$$\begin{split} u_{e_0} &= \sqrt{\frac{2\gamma}{\gamma - 1}} \frac{Q}{M_g} T_c \left[ 1 - \left(\frac{P_e}{P_c}\right)^{\frac{\gamma - 1}{\gamma}} \right] = \frac{3199}{3029} \text{ m/sec} \\ \text{and} \quad I_{sp_0} &= \frac{3199}{9.81} = \frac{326.1}{309.1} \text{ sec} \\ \end{split}$$
There is therefore a loss of  $\left( 1 - \frac{266.3}{326.1} \right) \times 100 = 18.3\%$  in  $I_{gp}$   
 $1 - \frac{257.3}{309.1}$ 

It is interesting to test the accuracy of the <u>linear</u> approximation given in class for small x:

$$\frac{u_e}{u_{e_0}} \simeq 1 - \frac{x}{2} \left[ 1 - \frac{c}{c_{pg}} \left( 1 + \frac{\left(1 - \eta_0\right) ln \left(1 - \eta_0\right)}{\eta_0} \right) \right]; \ \eta_0 = 1 - \left( \frac{P_e}{P_c} \right)^{\frac{\gamma - 1}{\gamma}}$$

We find  $\eta_0=0.4878$  , and then  $\frac{u_e}{u_{e_0}}=0.837$  (16.3% loss)

(not too different, despite large x)

NOTE: Alternatively, and easier to do, you can use

$$u_{e} = \sqrt{2\overline{C}_{p} T_{c} \left[1 - \left(\frac{P_{e}}{P_{c}}\right)^{\frac{\overline{\gamma}-1}{\overline{\gamma}}}\right]}$$

with  $\overline{C}_{p} = (1 - 0.37)3180 + 0.37 \times 1260 = 2469 \text{ J/Kg/K}$ 

(So  $\overline{M}$  is not really needed)

As a check,  $\frac{\overline{\gamma}}{\overline{\gamma}-1} \frac{R}{\overline{M}} = \frac{1.1336}{0.1336} \frac{8.314}{0.02857} = 2469 \text{ J/Kg/K as it should.}$