

## 6B.2 Eccentric-Disk Rheometer Flow [TWL]

$$a. \quad \nabla \underline{v} = \begin{pmatrix} 0 & W & 0 \\ -W & 0 & 0 \\ AW & 0 & 0 \end{pmatrix}; \quad (\nabla \underline{v})^t = \begin{pmatrix} 0 & -W & AW \\ W & 0 & 0 \\ 0 & 0 & 0 \end{pmatrix}$$

$$\underline{\gamma}_{(1)} = AW \begin{pmatrix} 0 & 0 & 1 \\ 0 & 0 & 0 \\ 1 & 0 & 0 \end{pmatrix}; \quad \{\underline{\gamma}_{(1)}, \underline{\gamma}_{(1)}\} = (AW)^2 \begin{pmatrix} 1 & 0 & 0 \\ 0 & 0 & 0 \\ 0 & 0 & 1 \end{pmatrix}$$

$$\underline{\gamma}_{(2)} = -\{(\nabla \underline{v})^t \cdot \underline{\gamma}_{(1)} + \underline{\gamma}_{(1)} \cdot (\nabla \underline{v})\}$$

$$= -\begin{pmatrix} 0 & -W & AW \\ W & 0 & 0 \\ 0 & 0 & 0 \end{pmatrix} \begin{pmatrix} 0 & 0 & 1 \\ 0 & 0 & 0 \\ 1 & 0 & 0 \end{pmatrix} AW - \begin{pmatrix} 0 & 0 & 1 \\ 0 & 0 & 0 \\ 1 & 0 & 0 \end{pmatrix} \begin{pmatrix} 0 & W & 0 \\ -W & 0 & 0 \\ AW & 0 & 0 \end{pmatrix} AW$$

$$= -\begin{pmatrix} 2AW & 0 & 0 \\ 0 & 0 & W \\ 0 & W & 0 \end{pmatrix} AW$$

$$\underline{\gamma}_{(3)} = -\{(\nabla \underline{v})^t \cdot \underline{\gamma}_{(2)} + \underline{\gamma}_{(2)} \cdot \nabla \underline{v}\}$$

$$= \begin{pmatrix} 0 & -W & AW \\ W & 0 & 0 \\ 0 & 0 & 0 \end{pmatrix} \begin{pmatrix} 2A & 0 & 0 \\ 0 & 0 & 1 \\ 0 & 1 & 0 \end{pmatrix} AW^2 + \begin{pmatrix} 2A & 0 & 0 \\ 0 & 0 & 1 \\ 0 & 1 & 0 \end{pmatrix} \begin{pmatrix} 0 & W & 0 \\ -W & 0 & 0 \\ AW & 0 & 0 \end{pmatrix} AW^3$$

$$= AW^3 \begin{pmatrix} 0 & 3A & -1 \\ 3A & 0 & 0 \\ -1 & 0 & 0 \end{pmatrix}$$

$$\{\underline{\gamma}_{(1)} \cdot \underline{\gamma}_{(2)} + \underline{\gamma}_{(2)} \cdot \underline{\gamma}_{(3)}\} = -A^2 W^3 \begin{pmatrix} 0 & 1 & 2A \\ 1 & 0 & 0 \\ 2A & 0 & 0 \end{pmatrix}$$

## 6B.2 (cont'd)

b. From Eq. 6.2-1 we get

$$\begin{aligned}\tau_{xz} = & -[b_1 AW + b_2(0) + b_{11}(0) + b_3(-AW^3) \\ & + b_{12}(-2A^3W^3) + b_{111}(2A^3W^3)]\end{aligned}$$

$$\begin{aligned}\tau_{yz} = & -[b_1(0) + b_2(-AW^2) + b_{11}(0) + b_3(0) \\ & + b_{12}(0) + b_{111}(0)] = b_2 AW^2\end{aligned}$$

$$c. \lim_{A \rightarrow 0} \left( -\frac{\tau_{xz}}{AW} \right) = \lim_{A \rightarrow 0} (b_1 - b_3 W^2 - 2b_{12} A^2 W^2 + 2b_{111} A^2 W^2) = b_1 - b_3 W^2$$

$$\lim_{A \rightarrow 0} \left( -\frac{\tau_{yz}}{AW} \right) = -b_2 W$$

### 6B.3 Complex Viscosity for Third-Order Fluid [JDS]

a) Small Ampl. Osc. Shear:

$$\underline{\underline{\gamma}}^{(1)} = \begin{pmatrix} 0 & 1 & 0 \\ 1 & 0 & 0 \\ 0 & 0 & 0 \end{pmatrix} \dot{\gamma}^0 \operatorname{Re}\{e^{i\omega t}\}$$

since  $\dot{\gamma}^0 \ll 1$ , keep terms 1st order in  $\dot{\gamma}^0$ :

$$\underline{\underline{\gamma}}^{(2)} = \begin{pmatrix} 0 & 1 & 0 \\ 1 & 0 & 0 \\ 0 & 0 & 0 \end{pmatrix} \dot{\gamma}^0 \operatorname{Re}\{i\omega e^{i\omega t}\} + \dots$$

$$\underline{\underline{\gamma}}^{(3)} = \begin{pmatrix} 0 & 1 & 0 \\ 1 & 0 & 0 \\ 0 & 0 & 0 \end{pmatrix} \dot{\gamma}^0 \operatorname{Re}\{-\omega^2 e^{i\omega t}\} + \dots$$

$\underline{\underline{\gamma}}^{(1)}, \underline{\underline{\gamma}}^{(1)}, \underline{\underline{\gamma}}^{(1)}, \underline{\underline{\gamma}}^{(2)}$  contain terms 2nd order in  $\dot{\gamma}^0$

3rd Order fluid:

$$\underline{\underline{\tau}} = -[b_1 \underline{\underline{\gamma}}^{(1)} + b_2 \underline{\underline{\gamma}}^{(2)} + b_3 \underline{\underline{\gamma}}^{(3)} + \dots]$$

$$\tau_{yx} = \dot{\gamma}^0 \operatorname{Re}\{\eta^* e^{i\omega t}\}$$

$$\therefore \eta^* = b_1 + b_2 \omega i - b_3 \omega^2$$

$$b) \eta' = \operatorname{Re}\{\eta^*\} = b_1 - b_3 \omega^2$$

$$\eta'' = -\operatorname{Im}\{\eta^*\} = -b_2 \omega$$

Fig. 3.4-4 : Predicts correct 1st Order correction  
to  $\eta'$  from N

Fig 3.4-5 : Predicts correct 1st Order correction  
to  $\eta''/\omega$

Fig 3.4-6: Same as above for  $\eta' \neq \eta''$

$$c) \lim_{\omega \rightarrow 0} \frac{\eta''/\omega}{\eta'} = -\frac{b_2}{b_1}$$

$$\text{From (6.2-5,6)}: \lim_{\gamma \rightarrow 0} \frac{\Psi_1}{2n} = -\frac{2b_2}{2b_1} = -\frac{b_2}{b_1}$$

d) No.

6.8.3 a) Small Amplitude Oscillatory Shear Flow:  $\dot{\gamma}^o \ll \tau$ , where

$$\underline{\underline{\gamma}}^{(1)} = \begin{bmatrix} 0 & 1 & 0 \\ 1 & 0 & 0 \\ 0 & 0 & 0 \end{bmatrix} \dot{\gamma}^o \operatorname{Re}\{e^{i\omega t}\}, \text{ keep terms only to order } \dot{\gamma}^o \text{ (others are too small.)}$$

$$\underline{\underline{\gamma}}^{(2)} = \begin{bmatrix} 0 & 1 & 0 \\ 1 & 0 & 0 \\ 0 & 0 & 0 \end{bmatrix} \dot{\gamma}^o \operatorname{Re}\{i\omega e^{i\omega t}\} + \text{terms 2nd order in } \dot{\gamma}^o$$

$$\underline{\underline{\gamma}}^{(3)} = \begin{bmatrix} 0 & 1 & 0 \\ 1 & 0 & 0 \\ 0 & 0 & 0 \end{bmatrix} \dot{\gamma}^o \operatorname{Re}\{-\omega^2 e^{i\omega t}\} + \dots$$

Note that  $\underline{\underline{\gamma}}^{(1)} \cdot \underline{\underline{\gamma}}^{(1)}$ ,  $\underline{\underline{\gamma}}^{(1)} \cdot \underline{\underline{\gamma}}^{(2)}$ , contain terms only 2nd or higher order  $\dot{\gamma}^o$

$$\underline{\underline{\gamma}} = -[b_1 \underline{\underline{\gamma}}^{(1)} + b_2 \underline{\underline{\gamma}}^{(2)} + b_3 \underline{\underline{\gamma}}^{(3)} + \dots]; \text{ 3rd order fluid, 1st order in } \dot{\gamma}^o$$

$$\uparrow \tau_{yx} = \dot{\gamma}^o \operatorname{Re}\{\eta^* e^{i\omega t}\} \rightarrow \eta^* = b_1 + b_2 \omega i - b_3 \omega^2$$

$$b) \eta' = \operatorname{Re}\{\eta^*\} = b_1 - b_2 \omega^2; \eta'' = -\operatorname{Im}\{\eta^*\} = -b_2 \omega$$

Fig 3.4-4 → Predicts the correct 1st order correction for  $\eta'$  from const. ⑩ predicts  $\eta''/\omega$ , that is a constant

Fig 3.4-5 → " " " " " " " " " " " "

Fig 3.4-6 → Same as above for  $\eta'$  &  $\eta''$

$$c) \lim_{\omega \rightarrow 0} \frac{\eta''/\omega}{\eta'} = -b_2/b_1; \text{ from Eqs. (6.2-5, 6): } \lim_{\dot{\gamma} \rightarrow 0} \frac{\eta_1}{2\eta} = \frac{-2b_2}{2b_1} = -$$

d) No,  $\eta_1 \neq 0$  only for non-linear VE.

## 6B.12 The Second-Order Fluid and the "Turntable Experiment" [RBB]

a.  $\underline{\underline{\gamma}}^{(1)}(t) = \begin{pmatrix} -\sin 2Wt & \cos 2Wt & 0 \\ \cos 2Wt & \sin 2Wt & 0 \\ 0 & 0 & 0 \end{pmatrix} \dot{\gamma}$

$$\xrightarrow{t=0} \begin{pmatrix} 0 & 1 & 0 \\ 1 & 0 & 0 \\ 0 & 0 & 0 \end{pmatrix} \dot{\gamma}$$

$$\left\{ \underline{\underline{\gamma}}^{(1)} \cdot \underline{\underline{\gamma}}^{(1)} \right\} = \begin{pmatrix} 1 & 0 & 0 \\ 0 & 1 & 0 \\ 0 & 0 & 0 \end{pmatrix} \dot{\gamma}^2 \quad \leftarrow \text{No "t" appears here.}$$

b.  $\frac{\partial \underline{\underline{\gamma}}^{(1)}}{\partial t} = \begin{pmatrix} -\cos 2Wt & -\sin 2Wt & 0 \\ -\sin 2Wt & \cos 2Wt & 0 \\ 0 & 0 & 0 \end{pmatrix} 2W\dot{\gamma}$

$$\xrightarrow{t=0} \begin{pmatrix} -1 & 0 & 0 \\ 0 & 1 & 0 \\ 0 & 0 & 0 \end{pmatrix} 2W\dot{\gamma}$$

$$\nabla \underline{\underline{v}} = \begin{pmatrix} -\dot{\gamma} \sin Wt \cos Wt & -\dot{\gamma} \sin^2 Wt + W & 0 \\ \dot{\gamma} \cos^2 Wt - W & \dot{\gamma} \sin Wt \cos Wt & 0 \\ 0 & 0 & 0 \end{pmatrix}$$

$$\underline{\underline{\omega}} = \nabla \underline{\underline{v}} - (\nabla \underline{\underline{v}})^T = \begin{pmatrix} 0 & -1 & 0 \\ 1 & 0 & 0 \\ 0 & 0 & 0 \end{pmatrix} (\dot{\gamma} - 2W)$$

c.  $\underline{\underline{\gamma}}^{(2)} = \frac{D \underline{\underline{\gamma}}^{(1)}}{Dt} - \{(\nabla \underline{\underline{v}})^T \cdot \underline{\underline{\gamma}}^{(1)} + \underline{\underline{\gamma}}^{(1)} \cdot \nabla \underline{\underline{v}}\}$

Since  $\nabla \underline{\underline{v}} = \frac{1}{2} (\underline{\underline{\gamma}}^{(1)} + \underline{\underline{\omega}})$  and  $(\nabla \underline{\underline{v}})^T = \frac{1}{2} (\underline{\underline{\gamma}}^{(1)} - \underline{\underline{\omega}})$   
we have:

$$\underline{\underline{\gamma}}^{(2)} = \frac{D \underline{\underline{\gamma}}^{(1)}}{Dt} - \left\{ \underline{\underline{\gamma}}^{(1)} \cdot \underline{\underline{\gamma}}^{(1)} \right\} + \frac{1}{2} \left\{ \underline{\underline{\omega}} \cdot \underline{\underline{\gamma}}^{(1)} - \underline{\underline{\gamma}}^{(1)} \cdot \underline{\underline{\omega}} \right\}$$

d. Note that for the flow under consideration

$$\{\underline{V} \cdot \nabla \underline{\gamma}_{(1)}\} = 0. \text{ Then:}$$

$$\underline{\gamma}_{(2)} \Big|_{t=0} = \begin{pmatrix} -1 & 0 & 0 \\ 0 & 1 & 0 \\ 0 & 0 & 0 \end{pmatrix} 2W\dot{\gamma} - \begin{pmatrix} 1 & 0 & 0 \\ 0 & 1 & 0 \\ 0 & 0 & 0 \end{pmatrix} \dot{\gamma}^2$$

$$+ \frac{1}{2} \begin{pmatrix} 0 & -1 & 0 \\ 1 & 0 & 0 \\ 0 & 0 & 0 \end{pmatrix} \begin{pmatrix} 0 & 1 & 0 \\ 1 & 0 & 0 \\ 0 & 0 & 0 \end{pmatrix} \dot{\gamma} (\dot{\gamma} - 2W)$$

$$- \frac{1}{2} \begin{pmatrix} 0 & 1 & 0 \\ 1 & 0 & 0 \\ 0 & 0 & 0 \end{pmatrix} \begin{pmatrix} 0 & -1 & 0 \\ 1 & 0 & 0 \\ 0 & 0 & 0 \end{pmatrix} \dot{\gamma} (\dot{\gamma} - 2W)$$

$$= \cancel{\begin{pmatrix} -1 & 0 & 0 \\ 0 & 1 & 0 \\ 0 & 0 & 0 \end{pmatrix}} 2W\dot{\gamma} - \begin{pmatrix} 1 & 0 & 0 \\ 0 & 1 & 0 \\ 0 & 0 & 0 \end{pmatrix} \dot{\gamma}^2$$

$$+ \cancel{\begin{pmatrix} -1 & 0 & 0 \\ 0 & 1 & 0 \\ 0 & 0 & 0 \end{pmatrix}} \dot{\gamma} (\dot{\gamma} - 2W)$$

$$= - \begin{pmatrix} 1 & 0 & 0 \\ 0 & 0 & 0 \\ 0 & 0 & 0 \end{pmatrix} 2\dot{\gamma}^2$$

from  $\frac{\partial \underline{\gamma}_{(1)}}{\partial t}$

from  $\underline{\gamma}_{(1)} \cdot \underline{\gamma}_{(1)}$

from  $\underline{w}$ -terms

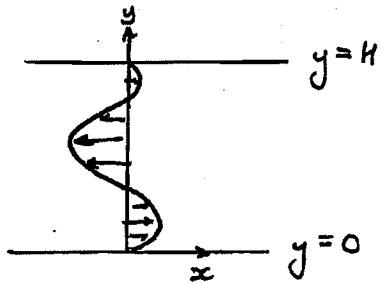
$$e. \begin{pmatrix} \tau_{xx} & \tau_{xy} & 0 \\ \tau_{yx} & \tau_{yy} & 0 \\ 0 & 0 & \tau_{zz} \end{pmatrix} = -b_1 \begin{pmatrix} 0 & 1 & 0 \\ 1 & 0 & 0 \\ 0 & 0 & 0 \end{pmatrix} \dot{\gamma}$$

$$+ b_2 \begin{pmatrix} 1 & 0 & 0 \\ 0 & 0 & 0 \\ 0 & 0 & 0 \end{pmatrix} 2\dot{\gamma}^2 - b_{11} \begin{pmatrix} 1 & 0 & 0 \\ 0 & 1 & 0 \\ 0 & 0 & 0 \end{pmatrix} \dot{\gamma}^2$$

This is the same as Eq. 6.2-4; there is no dependence on  $W$ .

f. If  $\underline{\gamma}_{(2)}$  is replaced by  $\frac{\partial \underline{\gamma}_{(1)}}{\partial t}$  in the above, there would be no  $\underline{w}$ -terms, and there would be a  $W$ -dependence!

## S.C.1 STABILITY OF SECOND ORDER FLUIDS [GHM]



$$\text{B.C. } v_x(0, t) = v_x(H, t) = 0$$

$$\text{I.C. } v_x(y, t) = u(y)$$

There is no modified pressure gradient and the flow is RECTILINEAR,  $v_y = v_z = 0$

a) The Velocity gradient tensor is  $\nabla v = \dot{\gamma} \begin{pmatrix} 0 & 0 & 0 \\ 1 & 0 & 0 \\ 0 & 0 & 0 \end{pmatrix}$  where  $\dot{\gamma} = \frac{\partial v_x}{\partial y}$

The Kinematic Tensors required for second order Fluid are

$$\underline{\underline{\gamma}}_{(1)} = \dot{\gamma} \begin{pmatrix} 0 & 1 & 0 \\ 1 & 0 & 0 \\ 0 & 0 & 0 \end{pmatrix} \quad \underline{\underline{\gamma}}_{(1)} : \underline{\underline{\gamma}}_{(1)} = 2\dot{\gamma}^2 \begin{pmatrix} 1 & 0 & 0 \\ 0 & 1 & 0 \\ 0 & 0 & 0 \end{pmatrix}$$

$$\underline{\underline{\gamma}}_{(2)} = \frac{\partial \dot{\gamma}}{\partial t} \begin{pmatrix} 0 & 1 & 0 \\ 1 & 0 & 0 \\ 0 & 0 & 0 \end{pmatrix} - 2\dot{\gamma}^2 \begin{pmatrix} 1 & 0 & 0 \\ 0 & 1 & 0 \\ 0 & 0 & 0 \end{pmatrix}$$

Hence

$$\underline{\underline{\tau}} = -b_1 \left[ \dot{\gamma} \begin{pmatrix} 0 & 1 & 0 \\ 1 & 0 & 0 \\ 0 & 0 & 0 \end{pmatrix} + \frac{b_2}{b_1} \begin{pmatrix} -2\dot{\gamma}^2 & \frac{\partial \dot{\gamma}}{\partial t} & 0 \\ \frac{\partial \dot{\gamma}}{\partial t} & 0 & 0 \\ 0 & 0 & 0 \end{pmatrix} + \frac{b_{11}}{b_1} \dot{\gamma}^2 \begin{pmatrix} 1 & 0 & 0 \\ 0 & 1 & 0 \\ 0 & 0 & 0 \end{pmatrix} \right]$$

The Cauchy Momentum Equation (in component form) is

$$x\text{-component } \rho \frac{\partial v_x}{\partial t} = - \frac{\partial \tau_{yx}}{\partial y} \quad \left\{ \begin{array}{l} \text{since } v_y = v_z = 0 \\ \text{and } \tau_{xyc} \neq f(x) \end{array} \right.$$

Substituting for  $\tau_{yx}$  from constitutive Eqn. gives

$$\rho \frac{\partial v_x}{\partial t} = + \frac{\partial}{\partial y} \left\{ b_1 \frac{\partial v_x}{\partial y} + b_2 \frac{\partial}{\partial t} \left( \frac{\partial v_x}{\partial y} \right) \right\}$$

Interchanging order gives

$$\boxed{\rho \frac{\partial v_x}{\partial t} = b_1 \left[ \frac{\partial^2 v_x}{\partial y^2} + \frac{b_2}{b_1} \frac{\partial}{\partial t} \left( \frac{\partial^2 v_x}{\partial y^2} \right) \right]} \quad (1)$$

b) Separation of Variables  $\Rightarrow$  postulate a solution  $v_{xc}(y, t) = Y(y)T(t)$

Solution satisfies homogeneous B.C's  $v_{xc}(0) = 0$   
 $v_{xc}(H) = 0$   
 Inhomogeneous I.C.  $v_{xc}(y, 0) = u(y)$

Substitution into ① gives

$$\frac{\rho T'}{b_1 \left[ T + \frac{b_2}{b_1} T' \right]} = \frac{Y''}{Y} = -K_n^2 \text{ say}$$

SPATIAL PART  $Y = \sum_{n=0}^{\infty} A_n \cos K_n y + B_n \sin K_n y$

Using B.C's  $y=0, v_{xc}=0 \Rightarrow Y=0 \Rightarrow A_n = 0$

$$y=H, v_{xc}=0 \Rightarrow Y=0 \Rightarrow K_n = \frac{n\pi}{H} \quad n=1, 2, \dots$$

TEMPORAL PART

rearranging gives  $T = -\left(\frac{b_2}{b_1} + \frac{\rho}{b_1 K_n^2}\right) T'$

define  $\alpha_n = -\left(\frac{b_2}{b_1} + \frac{\rho}{b_1 K_n^2}\right)^{-1} \Rightarrow \frac{dT}{dt} - \alpha_n T = 0$

$$\Rightarrow \underline{T(t)} = C_n e^{\alpha_n t}$$

Combining Solutions

$$\underline{v_{xc}(y, t)} = \sum_{n=1}^{\infty} \tilde{A}_n \sin\left(\frac{n\pi y}{H}\right) \exp(\alpha_n t)$$

where  $\tilde{A}_n \equiv (A_n C_n)$  and  $\alpha_n$  is given above

$\tilde{A}_n$  is determined from orthogonality and inhomogeneous initial data at  $t=0$

$$\begin{aligned} \int_0^H u(y) \sin\left(\frac{m\pi y}{H}\right) dy &= \int_0^H \left( \sum_{n=1}^{\infty} \tilde{A}_n \sin\left(\frac{n\pi y}{H}\right) \right) \sin\left(\frac{m\pi y}{H}\right) dy \\ &= \frac{\tilde{A}_m}{2} \delta_{mn} \end{aligned}$$

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